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**Albin**

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(54) **SYSTEM AND PROCESS FOR INJECTING CATALYST AND/OR ADDITIVES INTO A FLUIDIZED CATALYTIC CRACKING UNIT**

(58) **Field of Classification Search**  
USPC ..... 208/113, 152, 153, 164; 406/14, 109; 222/53

See application file for complete search history.

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(\*) Notice: Subject to any disclaimer, the term of this patent is extended or adjusted under 35 U.S.C. 154(b) by 739 days.

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(51) **Int. Cl.**

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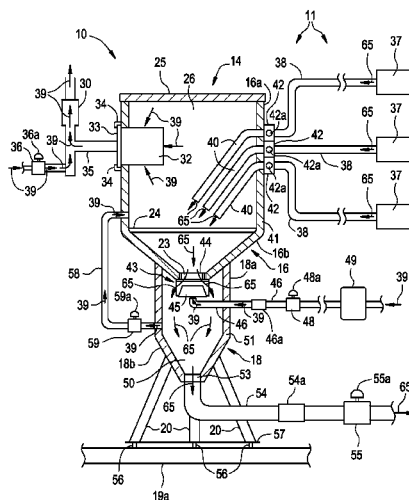
(52) **U.S. Cl.**

CPC ..... **C10G 11/18** (2013.01); **B01J 8/003** (2013.01); **B01J 8/004** (2013.01); **B01J 8/006** (2013.01); **B01J 8/0015** (2013.01); **B01J 8/0025** (2013.01); **B01J 8/0035** (2013.01); **B01J 8/06** (2013.01); **B01J 8/18** (2013.01); **B01J 8/24** (2013.01); **B01J 2208/00548** (2013.01); **B01J 2208/00752** (2013.01); **B01J 2208/00761** (2013.01); **B01J 2208/00769** (2013.01); **C10G 2300/80** (2013.01)

(57) **ABSTRACT**

A preferred embodiment of a system for loading catalyst and/or additives into a fluidized catalytic cracking unit includes a bin for storing at least one of the catalyst and/or additives, and a loading unit in fluid communication with the storage bin and the fluidized catalytic cracking unit on a selective basis. The loading unit is capable of being evacuated so that a resulting vacuum within the loading unit draws the catalyst and/or additive from the bin. The loading unit is also capable of being pressurized so that the catalyst and/or additive is transferred from the loading unit to the fluidized catalytic cracking unit.

**9 Claims, 8 Drawing Sheets**



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FIG. 1

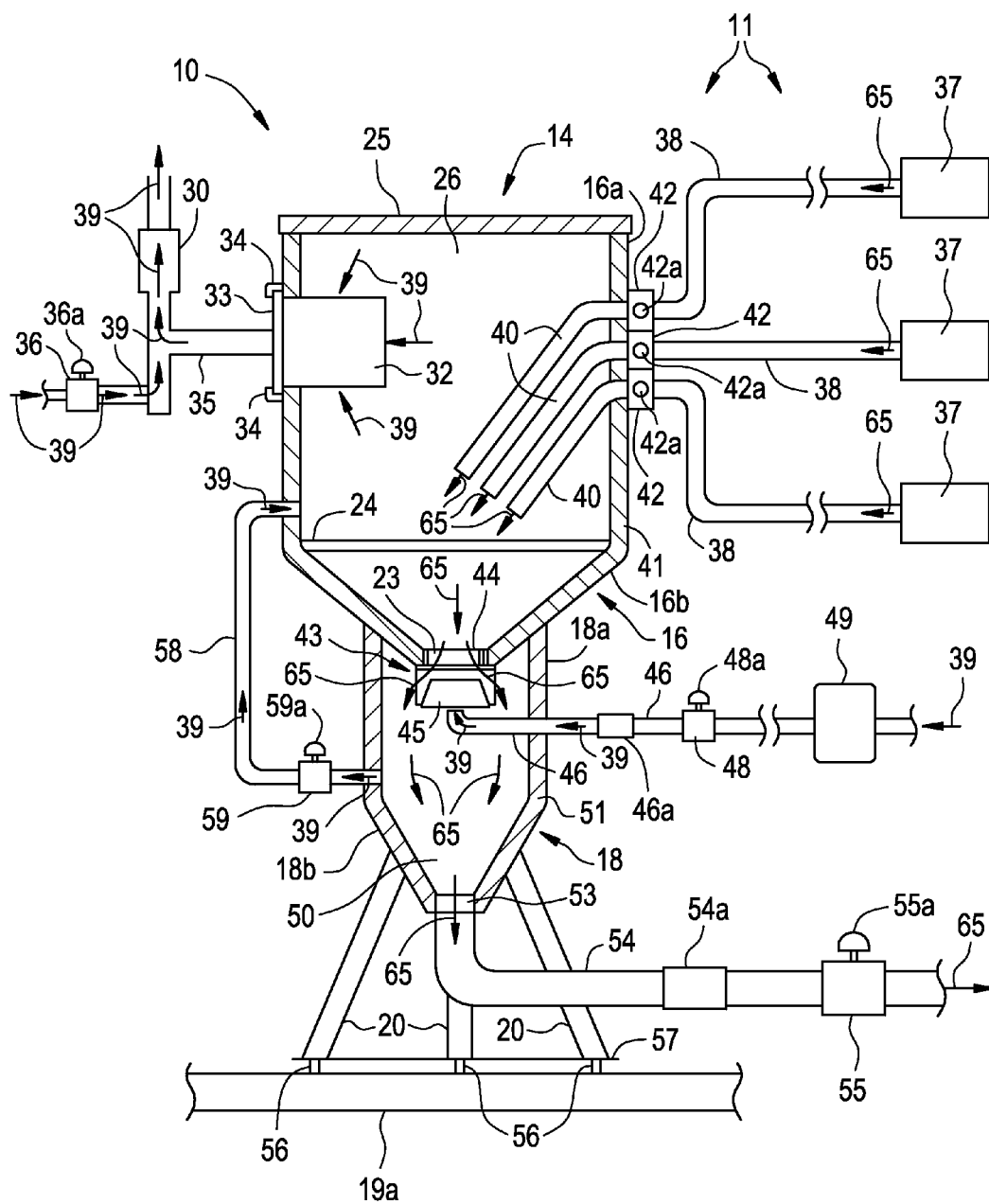


FIG. 2

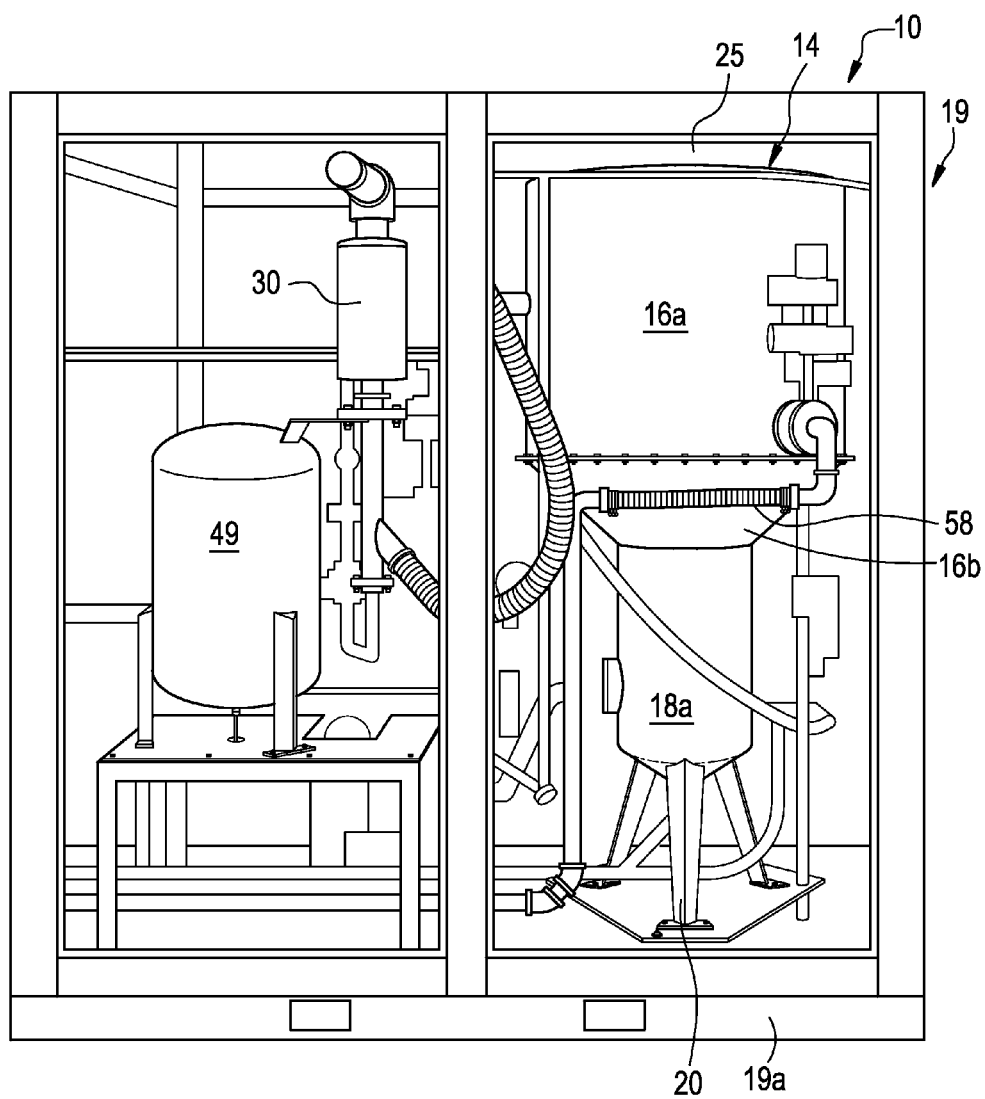


FIG. 3

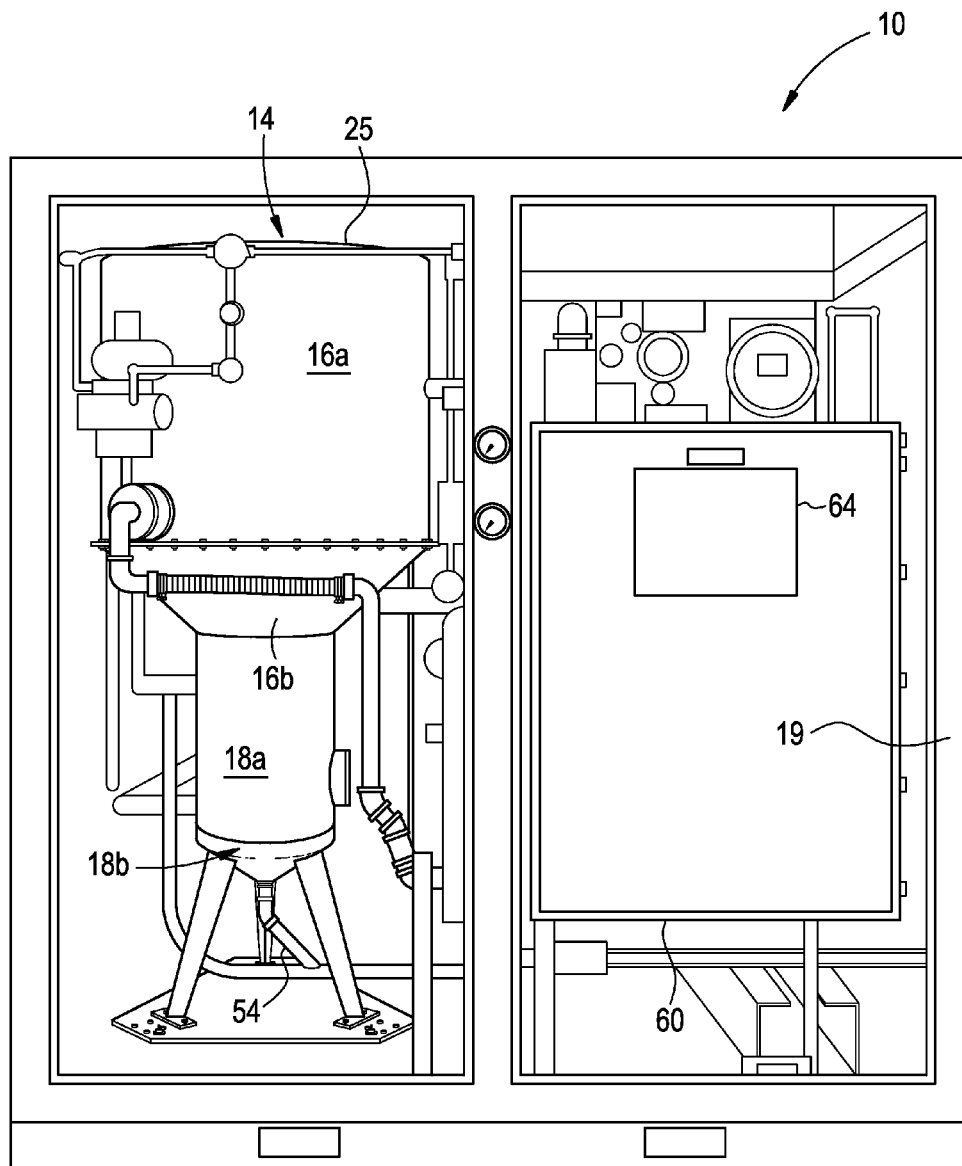


FIG. 4

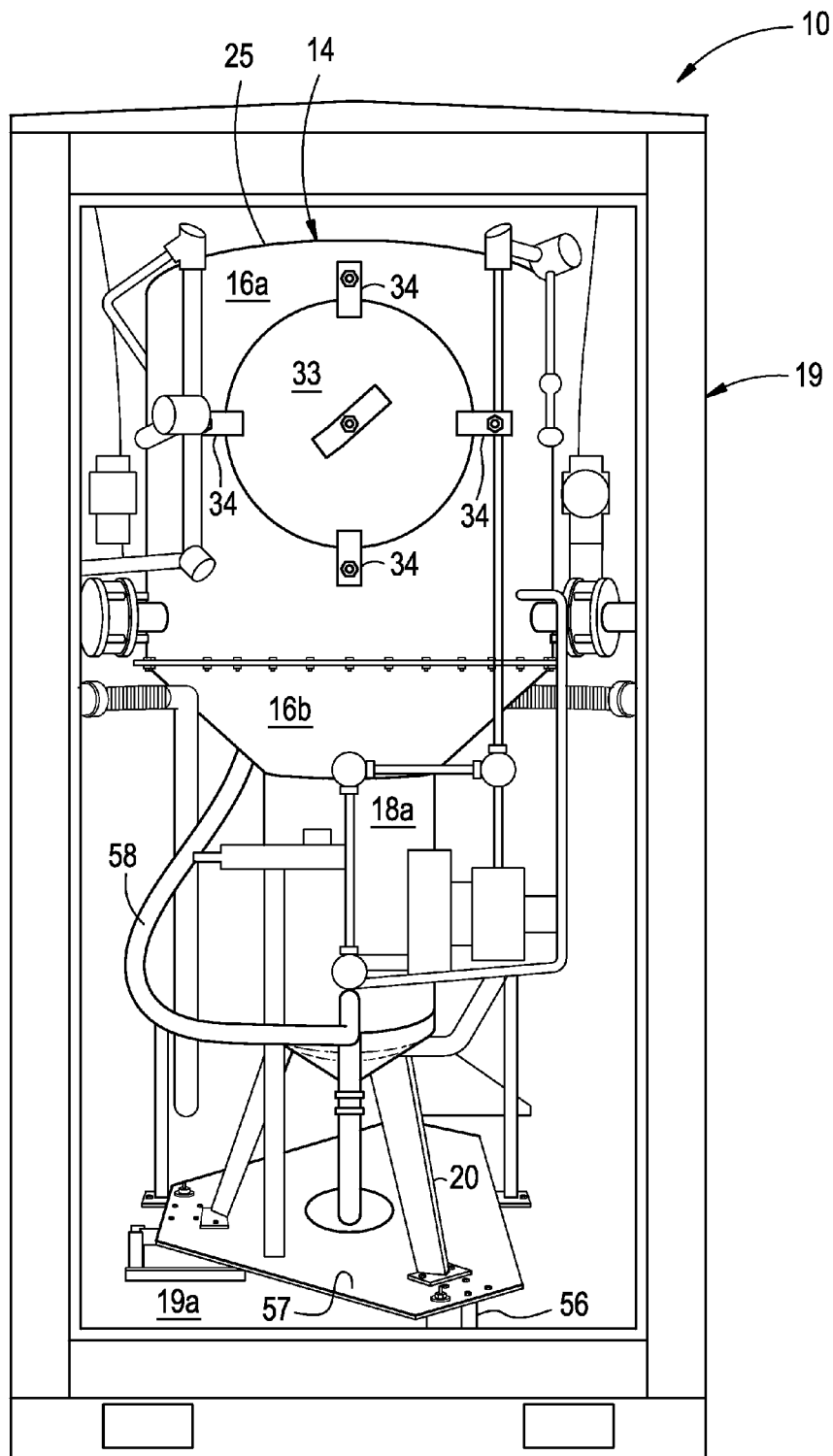


FIG. 5

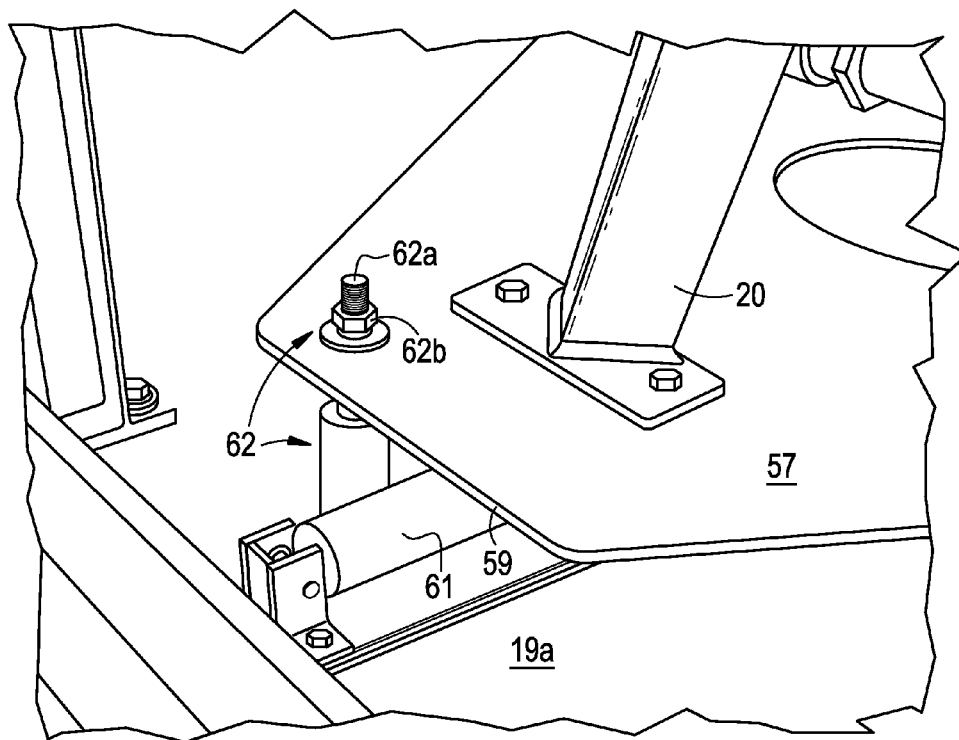


FIG. 6

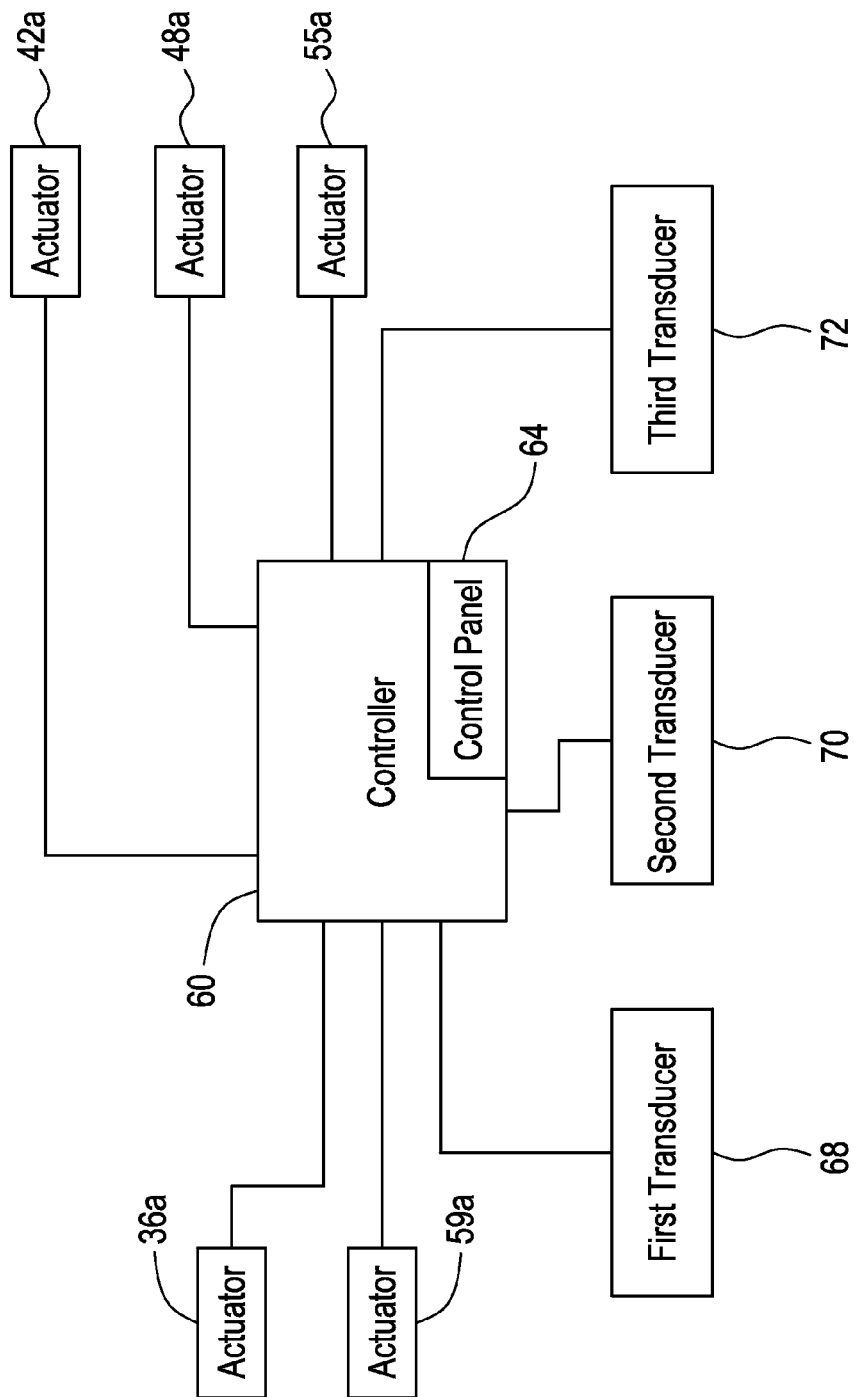




FIG. 7

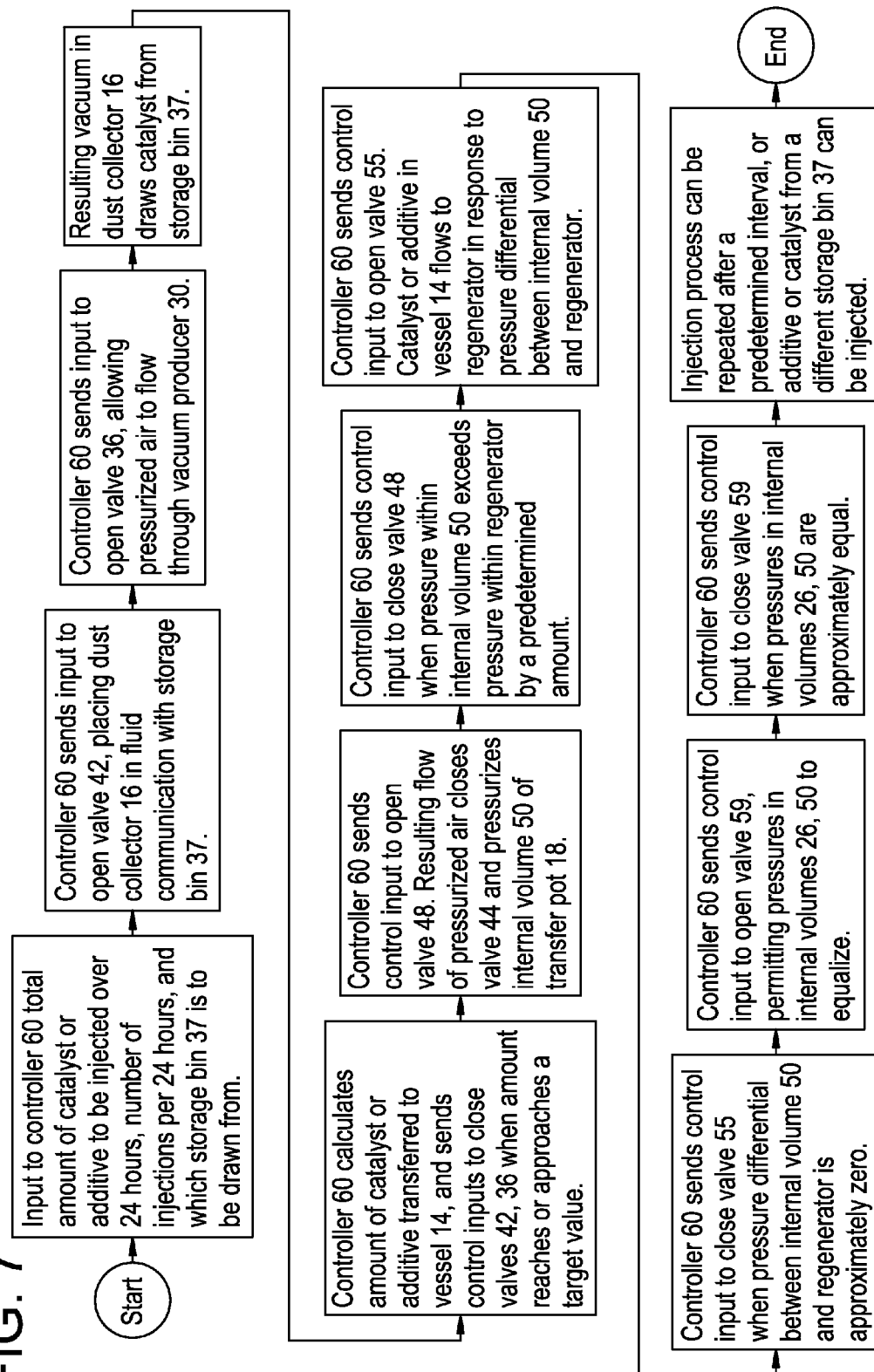
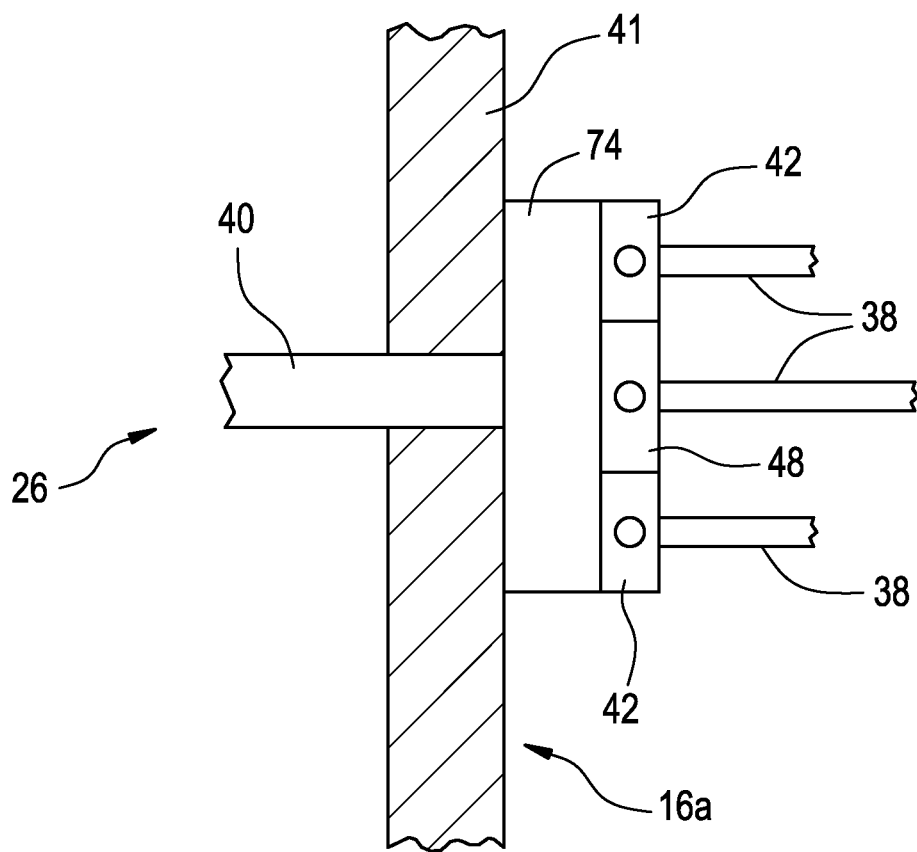


FIG. 8



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# SYSTEM AND PROCESS FOR INJECTING CATALYST AND/OR ADDITIVES INTO A FLUIDIZED CATALYTIC CRACKING UNIT

## CROSS REFERENCE OF THE INVENTION

This application is a divisional of U.S. patent application Ser. No. 10/806,563 filed on Mar. 23, 2004, the content of which is hereby incorporated by reference as if set forth in its entirety herein.

## FIELD OF THE INVENTION

The present invention relates to equipment used in fluidized catalytic cracking (FCC) operations and, more particularly, to systems and processes for injecting catalyst and/or additives into equipment units employed to conduct FCC operations.

## BACKGROUND OF THE INVENTION

FCC units commonly include a circulating inventory of bulk catalyst. The bulk catalyst is typically used to perform a primary function, such as producing naptha from petroleum feedstock, the naptha being further processed into gasoline. Additives, which are often in the same fluidizable and particulated form as the catalyst, are often introduced into the circulating inventory of bulk catalyst to perform a secondary function such as reducing certain types of emissions, e.g., SOx or NOx, produced by the FCC unit. These emissions are produced in the catalyst regenerator of the FCC unit where coke deposits from the cracked petroleum are burned off and the regenerated catalyst returned to the circulating catalyst inventory. These additives are usually introduced into the regenerator using an injection device commonly referred to as a "loader." Loaders are also used to add catalyst to the bulk inventory as additional catalyst becomes necessary due to factors such as attrition and deactivation.

Loaders used for catalyst and/or additive injection typically comprise a transfer pot, and a storage hopper or silo located above or proximate the transfer pot. The catalyst and/or additive is usually transferred to the storage hopper from a storage bin using a suitable technique such as vacuum transfer. During operation of the loader, a predetermined amount of catalyst and/or additive can be metered to the transfer pot from the storage hopper. The transfer pot can subsequently be pressurized, and the catalyst and/or additive can be injected into the regenerator in response to the pressure within the transfer pot. This process is usually repeated on a cyclical basis.

The amount of catalyst metered to the transfer pot and injected during each cycle is usually small in comparison to the overall volume of the storage hopper. In other words, a relatively large volume of catalyst and/or additive is typically stored in the hopper so that relatively small doses of the catalyst and/or additive can be metered to the transfer pot during each cycle. A typical storage hopper is relatively large due to the need to accommodate a large amount of additive or catalyst therein. For example, a typical storage hopper can have a diameter of five feet or more, and height of fifteen feet or more.

The relatively large size of conventional storage hoppers can limit the number of suitable locations in which the loader can be installed. This characteristic can be particularly disadvantageous at a refinery, where space can be and often is limited. The need for a relatively large area to accommodate

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the loader (and in particular the storage hopper) can thus necessitate placing the loader in a less than optimal location.

Moreover, the loader can only be used to inject one type of catalyst and/or additive at a time, due to the need for a dedicated storage hopper for each type of catalyst and/or additive. In other words, the transfer pot can only inject the catalyst and/or additive stored in its associated hopper, until the catalyst and/or additive is replaced with another type of catalyst and/or additive. Hence, loading different types catalyst and/or additives on simultaneous or near-simultaneous (back to back) basis can only be accomplished using multiple loaders. Each additional loader requires additional outlays of time, labor, and money to purchase, install, operate, and maintain. Moreover, each loader consumes potentially valuable space within the refinery.

The storage hopper may be pressurized in some applications to facilitate transfer of the catalyst and/or additive to the transfer pot. The pressurized air within the hopper can adversely affect the measurements that provide and indication of how much catalyst and/or additive has been added to the transfer pot. Also, the catalyst and/or additive may be exposed to pressurized air from the refinery (commonly referred to as "plant air") while it is being transferred to, or stored in the hopper. Plant air often contains moisture or other contaminants that can adversely affect the catalyst and/or additive.

## SUMMARY OF THE INVENTION

A preferred embodiment of a system for injecting catalyst and/or additives into a fluidized catalytic cracking unit comprises a dust collector in fluid communication with a storage bin holding one of the catalyst and/or additives, and a vacuum producer in fluid communication with the dust collector so that the vacuum producer generates a vacuum within the dust collector that draws the one of the catalyst and/or additives into the dust collector.

The system also comprises a transfer pot for receiving the one of the catalyst and/or additives from the dust collector. The transfer pot is in fluid communication with the fluidized catalytic cracking unit and a source of pressurized air so that the one of the catalyst and/or additives is transferred to the fluidized catalytic cracking unit in response to a pressure differential between the transfer pot and the fluidized catalytic cracking unit.

A preferred embodiment of a system for loading catalyst and/or additives into a fluidized catalytic cracking unit comprises a bin for storing at least one of the catalyst and/or additives, and a loading unit in fluid communication with the storage bin and the fluidized catalytic cracking unit on a selective basis. The loading unit is capable of being evacuated so that a resulting vacuum within the loading unit draws the at least one of the catalyst and/or additives from the bin, and the loading unit is capable of being pressurized so that the least one of the catalyst and/or additives is transferred from the loading unit to the fluidized catalytic cracking unit.

Another preferred embodiment of a system for loading catalyst and/or additives into a fluidized catalytic cracking unit comprises a first bin for storing a first of the catalyst and/or additives, a second bin for storing a second of the catalyst and/or additives, and a loading unit in fluid communication with the first and second bins and the fluidized catalytic cracking unit. The system also comprises a first valve for isolating the first bin from the loading unit on a selective basis, a second valve for isolating the second bin from the

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loading unit on a selective basis, and a third valve for isolating the second bin from the fluidized catalytic cracking unit on a selective basis.

A preferred embodiment of a system for introducing catalyst and/or additives into a fluidized catalytic cracking unit comprises a dust collecting means in fluid communication with a storage bin holding one of the catalyst and/or additives, and a vacuum producing means in fluid communication with the dust collecting means so that the vacuum producing means draws the one of the catalyst and/or additives into the dust collecting means. The system also comprises a means for receiving the one of the catalyst and/or additives from the dust collecting means and injecting the one of the catalyst and/or additives into the fluidized catalytic cracking unit.

A preferred process for introducing catalyst and/or additives into a fluidized catalytic cracking unit comprises generating a vacuum within a loading unit, drawing one of the catalyst and/or additives from a storage bin and into the loading unit in response to the vacuum, pressurizing the loading unit, and injecting the one of the catalyst and/or additives into the fluidized catalytic cracking unit in response to the pressurization of the loading unit.

A preferred process for loading catalyst and/or additives into a fluidized catalytic cracking unit comprises storing at least one of the catalyst and/or additives at a first location, vacuuming the at least one of the catalyst and/or additives into a loading unit positioned at a second location, and injecting the at least one of a catalyst and/or additives into the fluidized catalytic cracking unit from the loading unit.

A preferred embodiment of a system for introducing one or more particulate substances into a fluid stream comprises a dust collecting means in fluid communication with at least one storage bin holding the one or more particulate substances. The system also comprises a vacuum producing means in fluid communication with the dust collecting means so that the one or more particulate substances is drawn into the dust collecting means from the at least one storage bin by a vacuum. The system further comprises a means for receiving the one or more particulate substances from the dust collecting means and injecting the one or more particulate substances into the fluid stream.

#### BRIEF DESCRIPTION OF THE DRAWINGS

The foregoing summary, as well as the following detailed description of a preferred embodiment, are better understood when read in conjunction with the appended diagrammatic drawings. For the purpose of illustrating the invention, the drawings show an embodiment that is presently preferred. The invention is not limited, however, to the specific instrumentalities disclosed in the drawings. In the drawings:

FIG. 1 is a schematic side view of a preferred embodiment of a system for injecting catalyst and/or additives into an FCC unit, showing a dust collector and a transfer pot of the system longitudinal cross section;

FIG. 2 is a diagrammatic side view of the system shown in FIG. 1;

FIG. 3 is a diagrammatic side view of the system shown in FIGS. 1 and 2, from a perspective rotated approximately 180 degrees from the perspective of FIG. 2;

FIG. 4 is a diagrammatic side view of the system shown in FIGS. 1-3, from a perspective rotated approximately 90 degrees from the perspective of FIG. 2;

FIG. 5 is a magnified view of the area designated "A" in FIG. 3;

FIG. 6 is a block diagram depicting a control system of the system shown in FIGS. 1-5;

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FIG. 7 is a flow diagram depicting operation of the system shown in FIGS. 1-6; and

FIG. 8 is a top view of a manifold for use with an alternative embodiment of the system shown in FIGS. 1-6.

#### DESCRIPTION OF REFERRED EMBODIMENTS

A preferred embodiment of a system **10** for injecting catalyst and/or additives into an FCC unit is depicted in FIGS. 1-6. The loading system **10** forms part of an overall system **11** for storing and loading catalyst and/or additives. The system **11** includes the loading system **10**, and one or more storage bins **37**.

The loading system **10** comprises a loading unit **14** having a dust collector **16** and an adjoining transfer pot **18**. The loading system **10**, as discussed in detail below, produces a vacuum that draws catalyst and/or additive from the storage bins **37** and into the dust collector **16**. The catalyst and/or additive falls to the bottom of the dust collector **16** and into the transfer pot **18**. The transfer pot **18** is subsequently pressurized, and the catalyst and/or additive is injected into a regenerator of the FCC unit in response to the pressure within the transfer pot **18**.

The loading unit **14** can be housed within a cabinet **19** (see FIGS. 2-4). (The cabinet **19** is shown in the figures with its side panels removed, for clarity.) The loading unit **14** is preferably supported by a plurality of legs **20** affixed to the transfer pot **18**.

The dust collector **16** comprises a sidewall **17**. The sidewall **17** should be of a suitable strength and thickness to withstand the presence of a vacuum within the dust collector **16**.

The cross section and overall shape of the dust collector **16** can vary. The dust collector **16** depicted in the figures has a substantially cylindrical upper portion **16a**, and a substantially conical lower portion **16b** that adjoins the upper portion **16a**. An opening **23** is formed in the center of the lower portion **16b** (see FIG. 1). A screen **24** is positioned across the lower portion **16b**. In other embodiments, the cross section of the upper portion **16a** and the lower portion **16b** can be square or rectangular, and the overall shape can be in the form of a square or rectangular column. (Directional terms such as "upper," "lower," etc. are used herein with reference to the component orientations depicted in FIG. 1. These terms are used for exemplary purposes only, and are not intended to limit the scope of the appended claims.)

The dust collector **16** also includes a cover **25**. The cover **25** mates with an upper edge of the sidewall **17**. A gasket is positioned between the cover **25** and the sidewall **17** to form a substantially airtight seal therebetween. The sidewall **17** and the cover **25** define an internal volume **26** within the dust collector **16** (see FIG. 1).

The dust collector **16** also comprises a suitable filter **32** (see FIG. 1). The filter **32** can be, for example, a Mactiflo model E376094 filter.

The filter **32** is mounted within the upper portion **16a** of the dust collector **16**. The sidewall preferably includes a hatch **33** to provide access to the interior of the upper portion **16a** (and the filter **32**) (see FIGS. 1 and 4). The hatch **33** is preferably secured the sidewall **17** of the dust collector **16** using brackets **34** that permit the hatch **33** to be removed with a minimal expenditure of time and effort, thereby facilitating replacement of the filter **32** with a minimum of time and effort. Alternative embodiments of the loading system **10** can be equipped with more than one of the filters **32**.

The system **10** also comprises suitable vacuum producer **30** (see FIGS. 1 and 2). For example, the vacuum producer can be an Empire two-inch Vacutran S150 vacuum producer.

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The vacuum producer 30 is mounted within the cabinet 19 (see FIG. 2). The vacuum producer 30 is preferably mounted separately from the loading unit 14. The vacuum producer 30 is in fluid communication with the filter 32 by way of a hose 35.

The vacuum producer 30 is in fluid communication with a suitable source of pressurized air (not shown). (The source of pressurized air can be the plant air typically available at refineries.) The flow of pressurized air into the vacuum producer 30 can be regulated by a suitable valve 36 having an actuator 36a (see FIG. 1).

The vacuum producer 30 can operate in a manner commonly known to those skilled in the art of vacuum-chamber design. In particular, opening the valve 36 permits the pressurized air to flow through the vacuum producer 30. The flow of pressurized air through the vacuum producer 30 causes the vacuum producer 30 to draw air from the internal volume 26 of the dust collector 16, thereby generating a vacuum within the internal volume 26. (The vacuum producer 30 draws the air through the filter 32, thereby causing the dust collector 16 to collect the dust generated by the flow of catalyst and/or additive into the dust collector 16.) The respective directions of various airflows within the loading system 10 are denoted by arrows 39 in FIG. 1.

The loading system 10 draws catalyst and/or additive from storage bins in response to the vacuum within the internal volume 26. In particular, the dust collector 16 is in fluid communication with storage bins 37 (see FIG. 1). The storage bins 37 hold catalyst and/or additives to be injected into the FCC unit. The storage bins 37 can be, for example, the shipping containers used to transport the catalyst and/or additives to the refinery at which the loading system 10 is installed.

Each storage bin 37 is coupled to the dust collector 16 by a corresponding hose (or pipe) 38. A suitable valve 42 having an actuator 42a is located between each hose 38 and the dust collector 16. Each valve 42 isolates its associated storage bin 37 from the dust collector 16 on a selective basis. The valves 42 are installed on the upper portion 16a of the dust collector 16, and are in fluid communication with the internal volume 26 by way of corresponding openings formed in the upper portion 16a of the dust collector 16. (The hoses 38 and valves 42 thus form part of the system 11 for storing and loading catalyst and/or additives).

The hoses 38 can be coupled to the upper portion 16a by way of a common manifold 74 in alternative embodiments, as shown in FIG. 8.

The hoses 38 are preferably equipped with fittings that permit the hoses 38 to be readily removed from the dust collector 16 (or the manifold 74) and the storage bins 37.

Opening one of the valves 42 permits catalyst and/or additive to be drawn from the associated storage bin 37 by way of the associated hose 38, in response to the vacuum within the internal volume 26. The catalyst and/or additive is thus drawn directly from the storage bin 37 and into the loading system 10, without a need to load the catalyst and/or additive into a storage hopper.

The loading system 10 is depicted as being equipped with three sets of the valves 42 and hoses 38, for exemplary purposes only. Alternative embodiments can be equipped with more or less than three valves 42 and three hoses 38, and can draw catalyst and/or additive from more or less than three of the storage bins 37.

The storage bins 37 can be positioned at a location remote from the loading system 10. For example, the storage bins 37 can be located up to twenty feet from the loading system 10. (The maximum distance between the loading system 10 and the storage bins 37 is application dependent, and can vary

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with factors such as the capacity of the vacuum producer 30, the diameter of the hoses 38, etc. A particular value for this parameter is specified for exemplary purposes only.)

The dust collector 16 preferably includes three pipe guides 40. Each pipe guide 40 is in fluid communication with an associated one of the hoses 38.

The catalyst and/or additive drawn into the internal volume 26 by way of one of the pipe guides 40. The pipe guides 40 discharge the catalyst or additive proximate into the internal volume 26, proximate the screen 24.

It should be noted that the depiction of the system 11 in FIG. 1 is schematic in nature, and the relative positions of the various hoses, piping, etc. of the system 11 can be different than those depicted in FIG. 1. For example, the openings formed in the upper portion 16a of the dust collector 16 to accommodate the hoses 38 can be positioned around the circumference of the upper portion 16a, in lieu of the vertical arrangement depicted in FIG. 1.

The catalyst or additive drops toward the bottom of the dust collector 16, i.e., toward the lower portion 16b, after being discharged from the pipe guide 40 due to gravity. The catalyst and/or additive passes through the screen 24 as it drops (see FIG. 1). The mesh of the screen 24 is preferably chosen to block the passage of relatively large clumps or catalyst and/or additive (or foreign objects), while permitting relatively fine granules of catalyst and/or additive to flow freely there-through. The substantially conical shape of the lower portion 16b directs the catalyst and/or additive toward the opening 23 in the lower portion 16b.

The loading system 10 includes a valve 43 for covering and sealing the opening 23 on a selective basis. The valve 43 can be, for example, a plug valve comprising a seat 44 and plug 45. The seat 44 is secured to the lower portion 16b, around the periphery of the opening 23. The plug 45 is movable between an upper and a lower position (the plug 45 is depicted in its lower position in FIG. 1).

The valve 43 is actuated by pressurized air. The pressurized air is directed to the valve 43 by way of piping 46 that extends through the transfer pot 18. The flow of pressurized air into the piping 46 can be initiated and interrupted on a selective basis by a valve 48 in fluid communication with the piping 46. The valve 48a includes an actuator 48a.

The pressurized air impinges upon the plug 45 after exiting of the piping 46. More particularly, the pressurized air is directed to the interior of the plug 45, and urges the plug 45 into its closed position against the seat 44. The contact between the plug 45 and the seat 44 substantially seals the opening 23.

The plug 45 drops from its closed to its open position when the pressurized air is interrupted by closing the valve 48. The resulting gap between the plug 45 and the seat 44 permits catalyst and/or additive reaching the bottom of the lower portion 16b to pass through the opening 23 and into the transfer pot 18 (see FIG. 1).

The loading system 10 preferably includes a volume chamber and moisture trap 49 in fluid communication with the piping 46 (see FIGS. 1 and 2). The volume chamber and moisture trap 49 removes moisture from the pressurized air directed to the valve 43.

The transfer pot 18 comprises a sidewall 51. The sidewall 51 should be of a suitable strength and thickness to withstand pressurization of the transfer pot 18.

The cross section and overall shape of the transfer pot 18 can vary. The transfer pot 18 depicted in the figures has a substantially cylindrical upper portion 18a, and a substantially conical lower portion 18b that adjoins the upper portion 18a. The upper portion 18a and the lower portion 18b of the

transfer pot 18, and the lower portion 16b of the dust collector 16 define an internal volume 50 within the transfer pot 18 (see FIG. 1). (The lower portion 16b and the valve 43 thus form a boundary between the internal volume 26 of the dust collector 16 and the internal volume 50 of the transfer pot 18.)

An opening 53 is formed in the center of the lower portion 18a of the transfer pot 18. The transfer pot 18 is coupled to the regenerator of the FCC unit by piping 54. The piping 54 is in fluid communication with the opening 53. Catalyst and/or additive enters the piping 54 by way of the opening 53 and subsequently flows to the regenerator, as discussed below.

A valve 55 having an actuator 55a is installed in piping 54. The valve 55 permits the transfer pot 18 to be isolated from the regenerator on a selective basis. A suitable transfer pot 18 can be obtained, for example, by adapting a Clemtex, Inc. model 2452 six-cubic foot sandblasting pot, or a model 1648 two-cubic-foot sandblasting pot to mate with the dust collector 16. (The sandblasting pot can be mated with the dust collector 16 by securing the lower portion 16b of the dust collector 16 to the upper periphery of the sandblasting pot by a suitable means such as welding.)

The loading unit 14 is supported by a plurality of load cells 56 (see FIGS. 1 and 4). The load cells 56, as discussed below, provide a measure of the weight of the loading unit 14 in both an unloaded and loaded condition, i.e., with and without catalyst and/or additive therein. The load cells 56 are preferably mounted between a base 19a of the cabinet 19, and a plate 57 fixedly coupled to the legs 20 of the transfer pot 18.

Each load cell can be restrained from substantial horizontal movement by a corresponding restraint 61 (the restraints 61 are shown only in FIG. 5, for clarity.) Each restraint 61 is pivotally coupled to the base 19a of the cabinet 19.

The loading system 10 can include a plurality of jack assemblies 62 (the jack assemblies 62 are shown only in FIG. 5, for clarity.) Each jack assembly 62 comprises a threaded shaft 62a fixedly coupled to the base 19a of the cabinet 19. Two nuts 62b are threadably coupled to each shaft 62a. The nuts 62b are located above and below the plate 57. The lower nuts 62b can be raised so that the lower nuts 62b support the plate 57 (and the portion of the loading system 10 positioned on the plate 57). The upper nuts 62b can be lowered to lock the plate 57 in position, i.e., the plate 57 can be sandwiched between the upper and lower nuts 62b.

The jack assemblies 62 can thus substantially isolate the load cells 57 from the weight of the loading system 10. This feature can be used, for example, to protect the load cells 57 from being damaged by impact loads during shipping of the loading system 10.

External connections to the loading unit 14 are preferably configured so as to introduce a negligible tare into the load cell readings. For example, the piping 54 includes a flexible section 46a that substantially decouples the transfer pot 18 from the portion of the piping 54 connected to the regenerator, thereby minimizing any tare introduced into the load cell readings (see FIG. 1). The piping 46 likewise includes a flexible section 46a that substantially decouples the transfer pot 18 from the portion of the piping 46 connected to the plant-air equipment. Moreover, the hoses 35, 38 preferably have sufficient flexibility so that any tare introduced thereby is negligible.

The internal volume 26 of the dust collector 16 and the internal volume 50 of the transfer pot 18 are in fluid communication on a selective basis by way of piping 58. A valve 59 having an actuator 59a is located in the piping 58 to selectively open and close the path formed by the piping 58. The piping 58 is used to equalize the pressures within the internal volumes 26, 50, as discussed below.

The loading system 10 preferably comprises a controller 60 (see FIGS. 3 and 6). The actuators 36a, 42a, 48a, 55a, 59a of the respective valves 36, 42, 48, 55, 59 are electrically coupled to the controller 60. This feature permits the operation of the valves 36, 42, 48, 55, 59 to be controlled by the controller 60.

The controller 60 is a programmable loop controller (PLC), although virtually any type of computing device such as a minicomputer, microcomputer, etc. can be used as the controller 60 in alternative embodiments. A server or mainframe computer that controls other equipment and processes at the refinery in which the loading system 10 is operated can also be used to control the loading system 10 in the alternative.

The controller 60 can include a control panel 64 for inputting commands and operating data to the controller 60 (see FIGS. 3 and 6). The controller 60 and the control panel 64 can be mounted on the cabinet 19. The control panel 64 by itself, or both the control panel 64 and the controller 60 can be mounted at a convenient location remote from the remainder of the loading system 10 in alternative embodiments. For example, the control panel 64 can be mounted in a central control room of the refinery, thus allowing the operation of the loading system 10 to be controlled on a remote basis.

The controller 60 can be configured to cause a predetermined amount of catalyst and/or additive to be injected into the regenerator. The predetermined amount can be input to the controller 60 by the user via the control panel 64.

Moreover, the controller 60 can be configured to facilitate injection of the catalyst and/or additive on a cyclical basis. For example, the controller 60 can be programmed to facilitate the injection of a predetermined amount of additive over a twenty-four hour period, i.e., per day, using a predetermined number of discrete injections over that period. The operation of the loading system 10 over one such cycle is described below, and is depicted in the form of a flow diagram in FIG. 7.

(The controller 60 can also be configured to facilitate injection of the catalyst and/or additive on a non-cyclical basis. In other words, the controller 60 can be programmed to facilitate periodic injections of varying amounts of catalyst and/or additive.)

The total amount of catalyst and/or additive to be injected over the twenty-four hour period can be input to the controller 60 by the user using the control panel 64. The number of discrete injections to be performed per day can also be input by way of the control panel 64. (The controller 60 can be programmed to operate based on other inputs in alternative embodiments. For example, the controller 60 can be programmed to inject a predetermined amount of additive per cycle, using predetermined interval between injections.)

The controller 60 can be programmed to automatically calculate the amount of catalyst and/or additive to be injected during each cycle based on the above-noted inputs. The controller 60 can also be programmed to calculate the time interval between the start of each injection. The interval is calculated by dividing twenty-four hours by the required number of injections per day. Moreover, the controller 60 can be configured to accept an input denoting the particular storage bin 37 from which the catalyst and/or additive is to be drawn.

The controller 60 sends a control input to the actuator 42a of the valve 42 associated with the particular storage bin 37 from which the catalyst and/or additive is to be drawn (see FIG. 7). The control input causes the actuator 42a to open the valve 42, thereby placing the storage bin 37 in fluid communication with the dust collector 16. (The valves 36, 42, 48, 55, 59 are in their respective closed positions, and the plug 45 of the valve 43 is in its open (lower) position at the start of the cycle.)

The controller 60 also sends an input to the actuator 36a of the valve 36, thereby allowing pressurized air to flow through the vacuum producer 30. The vacuum producer 30 creates a vacuum within the internal volume 26 of the dust collector 16 in response to the flow of pressurized air therethrough, as discussed above.

The vacuum within the internal volume 26 draws the catalyst and/or additive from the storage bin 37 and into the upper portion 16a of the dust collector 16. (The direction of travel of the catalyst and/or additive through the loading system 10 is denoted by arrows 65 in FIG. 1.) The catalyst and/or additive subsequently falls toward the lower portion 16b due to gravity, and enters the transfer pot 18 by way of the opening 23 in the lower portion 16b, as noted previously.

The controller 60 continually monitors the weight of the loading unit 14, and the weight of the catalyst and/or additive added thereto. (The combined weight of the loading unit 14 and any catalyst and/or additive therein is hereinafter referred to as the "live weight" of the loading system 10). In particular, the load cells 56 are electrically coupled to the controller 60. The controller 60 receives inputs from each of the load cells 56, and adds the inputs to determine the live weight of the loading system 10.

The controller 60 calculates the amount of catalyst and/or additive that is added to the loading system 10. The controller 60 performs this calculation by subtracting the live weight of the loading system 10 at a given instant from the live weight of the loading system 10 at the start of the cycle, i.e., immediately prior to the opening of the valves 36, 42 (the loading unit 14 is assumed to be substantially empty of catalyst and/or additive at the start of the cycle).

The controller 60 stops the flow of catalyst and/or additive to the dust collector 16 as the amount of catalyst and/or additive added to the loading system 10 approaches the amount to be injected into the regenerator during each cycle (this amount is subsequently referred to as a "target value"). In particular, the controller 60 sends a control input to the actuator 42a of the valve 42 as the weight of the catalyst of additive approaches its target value. The control input causes the valve 42 to close, thereby interrupting the flow of catalyst and/or additive to the dust collector 16. (The controller 60 can be programmed to commence the closing of the valve 42 when the weight of the catalyst and/or additive is below the target weight by a predetermined amount, so as to compensate for the lag between the issuance of the "close" command to the valve 42, and the point at which the valve 42 is fully closed).

The controller 60 also sends a control input to the actuator 36a of the valve 36 as the weight of the catalyst of additive in the loading system 10 reaches its target value. The control input causes the actuator 36a to close the valve 36, thereby interrupting the flow of pressurized air through the vacuum producer 30.

The controller 60 subsequently sends a control input to the actuator 48a of the valve 48 to cause the valve 48 to open. Opening the valve 48 permits pressurized air to enter the internal volume 50 of the transfer pot by way of the piping 46. The pressurized air impinges on the plug 45 of the valve 43 upon exiting the piping 46, and thereby urges the plug 45 into its closed (upper) position against the lower portion 16b of the dust collector 16, as discussed above. The contact between the plug 45 and the lower portion 16b covers and seals the opening 23.

The pressurized air pressurizes the internal volume 50 of the transfer pot 18 after the opening 23 has been sealed by the plug 45. (The pressurized air, as discussed above, is dried by the volume chamber and moisture trap 49 before reaching the

transfer pot 18, thereby minimizing the potential for contamination of the catalyst and/or additive within the transfer pot 18.)

The controller 60 receives an input from a first pressure transducer 68 that measures the pneumatic pressure in the internal volume 50 (see FIG. 6). The controller 60 also receives an input from a second pressure transducer 70 that measures the pneumatic pressure in the regenerator proximate the location at which the catalyst and/or additive is injected.

The controller 60 sends a control input to the actuator 48a of the valve 48 when the difference between the pneumatic pressures in the internal volume 50 and the regenerator 14 reaches a predetermined value, i.e., when the pressure in the internal volume 50 exceeds the pressure in the regenerator by a predetermined amount. This control input causes the valve 48 to close.

The controller 60 subsequently sends a control input to the actuator 55a of the valve 55 to cause the valve 55 to open. The differential between the pressures in the internal volume 50 and the regenerator causes the catalyst and/or additive in the transfer pot 18 to flow into the regenerator by way of the piping 54.

The controller 60 sends a control input to the actuator 55a to close the valve 55, after a predetermined interval has passed following issuance of the control input to open the valve 55. (The predetermined interval should be chosen so as to allow sufficient time for substantially all of the catalyst and/or additive in the transfer pot 18 to be injected into the regenerator).

The controller 60 subsequently sends a control input to the actuator 59a of the valve 59 to cause the valve 59 to open. The opening of the valve 59 permits the pneumatic pressures within the internal volumes 26, 50 to substantially equalize. In particular, opening the valve 59 relieves the relatively high pressure in the internal volume 50 (which is approximately equal to pressure within the regenerator 14) by way of the piping 58.

The controller 60 sends a control input to the actuator 59a of the valve 59 when the pressure differential between the internal volumes 26, 50 is approximately zero (the pneumatic pressure in the internal volume 26 can be measured by a third pressure transducer 72 located therein). This control input causes the valve 59 to close.

The controller 60 can be programmed to repeat the above process after the calculated interval between the start of each injection cycle (discussed above) has passed.

Moreover, the controller 60 can be programmed to inject catalyst and/or additive from any of the other storage bins 37 after the above-described cycle has been completed. In other words, another injection cycle can be performed in a manner identical to that described above, with the exception that the valve 42 associated with one of the other storage bins 37 can be opened to allow the catalyst and/or additive from that particular storage bin 37 to be drawn into the dust collector 16.

Vacuuming the catalyst and/or additive directly from its storage bin 37 can provide substantial flexibility in the operation of the loading system 10. For example, the loading system 10 can draw catalyst and/or additive from virtually any location at the refinery accessible by a hose such as the hose 38. Hence, the storage bins 37 can be positioned at an optimal location within the refinery. Moreover, the use of vacuum as a means to transport the catalyst and/or additive to the loading system 10 can permit the catalyst and/or additive to be drawn directly from its shipping container. Hence, the expenditure of time and labor associated with transferring the catalyst

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and/or additive from its shipping container to a storage unit can be eliminated through the use of the loading system 10.

Moreover, vacuuming the catalyst and/or additive directly into the dust collector 16 can obviate the need to transfer the catalyst and/or additive into a relatively large storage hopper (as is typically required with conventional loaders). Hence, the expenditure of time and labor associated with transferring the catalyst and/or additive to a storage hopper can be eliminated through the use of the loading system 10.

Eliminating the need for a storage hopper can also minimize the amount of spaced needed to accommodate the loading system 10. For example, the footprint the loading system 10 is approximately four feet by four feet, and the maximum height of the loading system is approximately five feet. A conventional loader of comparable capacity (with its storage hopper) can have a footprint of approximately five feet by eight feet, and a height of approximately twenty feet. (The dimensions of the loading system 10 will vary by application, and specific dimensions are provided herein for exemplary purposes only.) Moreover, in contradistinction to many conventional loaders, the loading system 10 can be installed without the use of special mounting provisions such as a base specifically tailored to a particular installation.

The loading system 10 can be repositioned with relative ease due to the absence of a storage hopper. In particular, the absence of a storage hopper provides a measure of portability to the loading system 10, and can facilitate movement of the loading system 10 between different locations within the refinery (or between different refineries) with a minimal expenditure of time and effort in comparison to conventional loaders. Portability and ease of use for the user of the loading system 10 is further enhanced when the loading system 10 is used in conjunction with portable storage bins, e.g., known as "totes," which are normally built to hold approximately 2,000 pounds (approximately 900 kilograms) of catalyst and/or additive.

The absence of a storage hopper, it is believed, can also minimize the amount of time necessary to install the loading system 10 in relation to conventional loaders. The ability to install the loading system 10 in a minimal amount of time can be particularly beneficial, for example, where the use of the loading system 10 is required on an immediate basis to comply with a particular regulatory standard.

The loading system 10 can be used to inject different types of catalyst and/or additives with no mechanical reconfiguration, and without the need to unload and reload a storage hopper. In particular, the loading system 10 can inject one type of catalyst and/or additive from one of the storage bins 37, and can immediately thereafter inject another type of catalyst from another of the storage bins 37 by manipulating the valves 42 in the appropriate manner. The need for multiple loaders to inject different types of catalyst and/or additives can thus be eliminated through the use of the loading system 10. It is believed that that substantial savings in time, labor, refinery space, and money can be achieved by eliminating the need to purchase, install, and maintain multiple loaders each dedicated to a particular type of catalyst and/or additive.

Eliminating the use of a storage hopper can also reduce the amount of moisture to which the catalyst and/or additive is exposed. In particular, the use of the loading system 10 permits the catalyst and/or additive to remain in the storage bins 37 until a point immediately prior to its injection into the regenerator 14. The environment in the storage bins 37, it is believed, can be controlled more closely than that within a storage hopper. In particular, catalyst and/or additive is typically exposed to plant air when being transported to and stored in a hopper. Plant air is often a source of moisture or

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other contamination that can adversely affect catalyst and/or additive. Hence, minimizing the exposure of the catalyst and/or additive to plant air, as in the loading system 10, can reduce the potential for contamination of the catalyst and/or additive.

The pressurized volume loading system 10 is believed to be less that of conventional loaders of comparable capacity. Hence, less pressurized air is required to operate the loading system 10 in comparison to conventional loaders. This feature can reduce the operating cost of the loading system 10 in relation to conventional loaders.

The loading unit 14 is substantially isolated from sources of pressurized air as the catalyst and/or additive is transferred thereto, due primarily to the use of a vacuum to transfer the catalyst and/or additive. Hence, the potential for the readings of the load cells 56 to be biased by forces induced by pressurized air is believed to be minimal. (Some types of conventional loaders, as discussed above, transfer catalyst and/or additive under pressure from a storage hopper to a transport unit. The pressurized air used effect the transfer can adversely affect readings of the transfer pot's weight.)

The foregoing description is provided for the purpose of explanation and is not to be construed as limiting the invention. While the invention has been described with reference to preferred embodiments or preferred methods, it is understood that the words which have been used herein are words of description and illustration, rather than words of limitation. Furthermore, although the invention has been described herein with reference to particular structure, methods, and embodiments, the invention is not intended to be limited to the particulars disclosed herein, as the invention extends to all structures, methods and uses that are within the scope of the appended claims. Those skilled in the relevant art, having the benefit of the teachings of this specification, may effect numerous modifications to the invention as described herein, and changes may be made without departing from the scope and spirit of the invention as defined by the appended claims.

## PARTS LIST

40 Loading system 10  
System 11 for storing and loading catalyst and/or additives  
Loading unit 14  
Dust collector 16  
Upper portion 16a (of dust collector 16)  
45 Lower portion 16b  
Sidewall 17 (of dust collector 16)  
Transfer pot 18  
Cabinet 19  
Base 19a (of cabinet 19)  
50 Legs 20 (on loading unit 14)  
Opening 23 (in lower portion 16b)  
Screen 24  
Cover 25  
Internal volume 26 (within dust collector 16)  
55 Vacuum producer 30  
Filter 32  
Hatch 33 (in dust collector 16)  
Brackets 34  
Hose 35  
60 Valve 36  
Actuator 36a (of valve 36)  
Storage bins 37  
Hoses 38  
Arrows 39  
65 Guide pipes 40  
Valve 42  
Actuator 42a (of valve 42)



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Valve 43  
 Seat 44  
 Plug 45 (of valve 43)  
 Piping 46  
 Flexible section 46a (of piping 46)  
 Valve 48  
 Actuator 48a (of valve 48)  
 Volume chamber and moisture trap 49  
 Internal volume 50 (within transfer pot 18)  
 Sidewall 51 (of transfer pot 18)  
 Opening 53 (in lower portion 18a of transfer pot 18)  
 Piping 54  
 Flexible section 54a (of piping 54)  
 Valve 55  
 Actuator 55a (of valve 55)  
 Load cells 56  
 Plate 57  
 Piping 58  
 Valve 59  
 Controller 60  
 Brackets 61  
 Jack assemblies 62  
 Shafts 62a (of jack assemblies 62)  
 Nuts 62b  
 Control panel 64 (of controller 60)  
 Arrows 65  
 First pressure transducer 68  
 Second pressure transducer 70  
 Third pressure transducer 72  
 Manifold 74

What is claimed is:

1. A process for introducing catalyst and/or additives into a fluidized catalytic cracking unit, comprising:

generating a vacuum within a loading unit;

drawing one of the catalyst and/or additives from a storage bin and into the loading unit in response to the vacuum wherein drawing one of the catalyst and/or additives from a storage bin and into the loading unit in response to the vacuum comprises opening a valve to place the storage bin in fluid communication with the loading unit;

drawing another catalyst and/or additive from another storage bin and into the loading unit in response to the vacuum by opening another valve to place the another storage bin in fluid communication with the loading unit;

monitoring the weight of the catalyst and/or additives drawn into the loading unit and stopping generation of the vacuum when the weight reaches a predetermined value;

pressurizing the loading unit; and

injecting the catalyst and/or additives into the fluidized catalytic cracking unit in response to the pressurization of the loading unit.

2. The process of claim 1, wherein generating a vacuum within a unit comprises initiating a flow of pressurized air through a vacuum producer in fluid communication with the loading unit.

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3. The process of claim 1, wherein injecting the one of the catalyst and/or additives into the fluidized catalytic cracking unit in response to the pressurization of the loading unit comprises injecting the one of the catalyst and/or additive into a regenerator of the fluidized catalytic cracking unit.

4. The process of claim 1, wherein pressurizing the loading unit comprises opening a valve to place the loading unit in fluid communication with a source of pressurized air.

5. The process of claim 1, wherein generating a vacuum within a unit and drawing one of the catalyst and/or additives from a storage bin and into the loading unit in response to the vacuum comprises generating the vacuum in a dust collector of the loading unit and drawing one of the catalyst and/or additives from a storage bin and into the dust collector in response to the vacuum.

6. The process of claim 1, wherein pressurizing the loading unit and injecting the one of the catalyst and/or additives into the fluidized catalytic cracking unit in response to the pressurization of the loading unit comprises pressurizing a transfer pot of the loading unit and injecting the one of the catalyst and/or additives into the fluidized catalytic cracking unit from the transfer pot.

7. A process for introducing at least two catalysts and/or additives into a fluidized catalytic cracking unit, each of said at least two catalysts and/or additives being stored in separate storage bins, the process comprising:

generating a vacuum within a loading unit;

opening a first valve to place a first storage bin holding one of the at least two catalysts and/or additives in fluid communication with the loading unit to draw the catalyst or additive from the first storage bin and into the loading unit in response to the vacuum;

opening a second valve to place a second storage bin holding at least one other catalyst or additive in fluid communication with the loading unit to draw the catalyst or additive from the second storage bin and into the loading unit in response to the vacuum;

pressurizing the loading unit; and

injecting the catalyst and/or additive from the loading unit into the fluidized catalytic cracking unit in response to the pressurization of the loading unit.

8. The process of claim 7 further comprising monitoring the weight of each of the at least two catalysts and/or additives drawn into the loading unit, and stopping the drawing of each of said catalyst and/or additive when the weight of the catalyst and/or additive drawn into the loading unit reaches a predetermined level.

9. The process of claim 7, wherein pressurizing the loading unit and injecting the catalyst and/or additives into the fluidized catalytic cracking unit in response to the pressurization of the loading unit comprises pressurizing a transfer pot of the loading unit and injecting the catalyst and/or additives into the fluidized catalytic cracking unit from the transfer pot.

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